

# 12-5 hydrogen production and energy storage

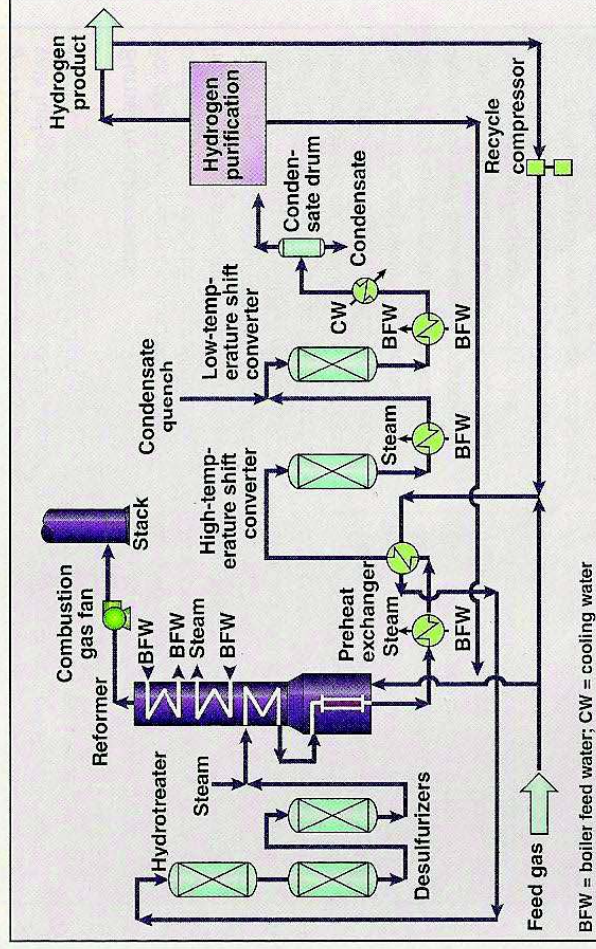
- technical processes and cost

# Hydrogen Production By Steam Reforming

**Management of the gas  
is critical for  
petroleum refiners**

Ray Elshout  
Energy Systems Engineering

Steam reforming of natural gas at petroleum refining facilities is the predominant means of producing hydrogen in the chemical process industries (CPI). Areas where hydrogen is heavily consumed include ammonia production, the cryogenics industry and methanol production (Table 1)[7]. Because hydrogen needs within various sectors of the CPI are at their highest



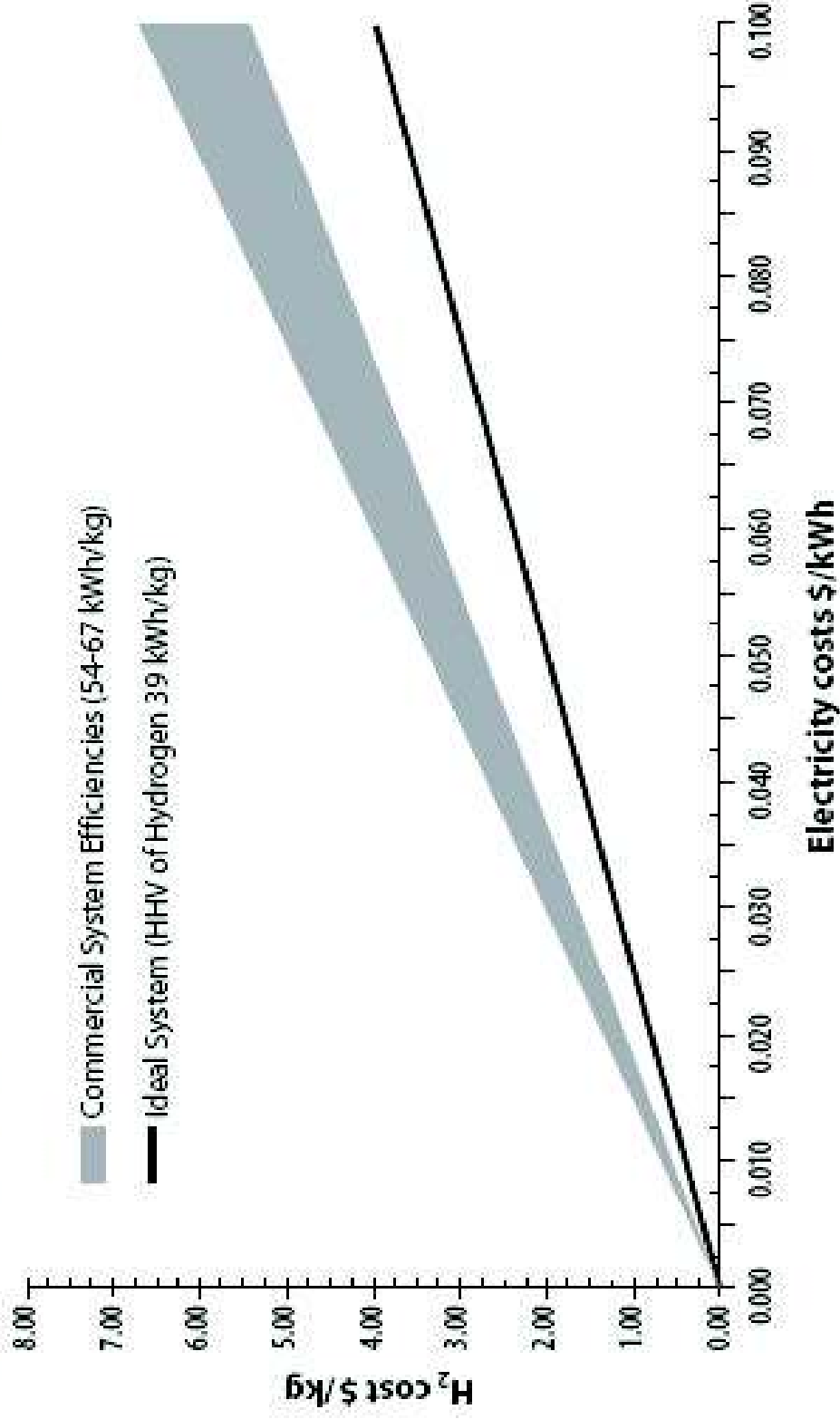
**FIGURE 1. Steam-methane reforming is still responsible for the bulk of hydrogen production in petroleum refineries**

diesel fuel. Management of hydrogen is | hydrogen from the users remaining

# NREL ( DOE)

## National Renewable Energy Laboratory

Figure 1. Hydrogen costs via electrolysis with electricity costs only



# Hydrogen cost

- To day the cheaper hydrogen is produced by **steam-methane reforming**
- $\text{CH}_4 + \text{H}_2\text{O} \rightarrow \text{CO} + 3\text{H}_2$  (755-1080K)  $\Delta = 206\text{MJ}$
- from CH4 Cost 400\$/T
- **Hydrogen from electrolysis : 1800-2000\$/T** for an electrical power at 50\$/MWh

# efficiency of the electrolyser for hydrogen production

- CEA/ENSMP thesis R.Rivera-Tinoco 30 march 2009
- conversion rate:
- 75% at high temperature electrolysis (EPR temperature)
- NREL (innovation for our energy future)-DOE
- **water to hydrogen conversion efficiency:80 to 95%**
- 56% for Proton's proton exchange membrane(PEM)
- 73% for Stuart's and Norsk Hydro's bipolar alkaline systems
- 64% for Avalence and Teledyne units
- **75% to 85% second generation of solid oxide electrolyser cells (SOECs)**
- -

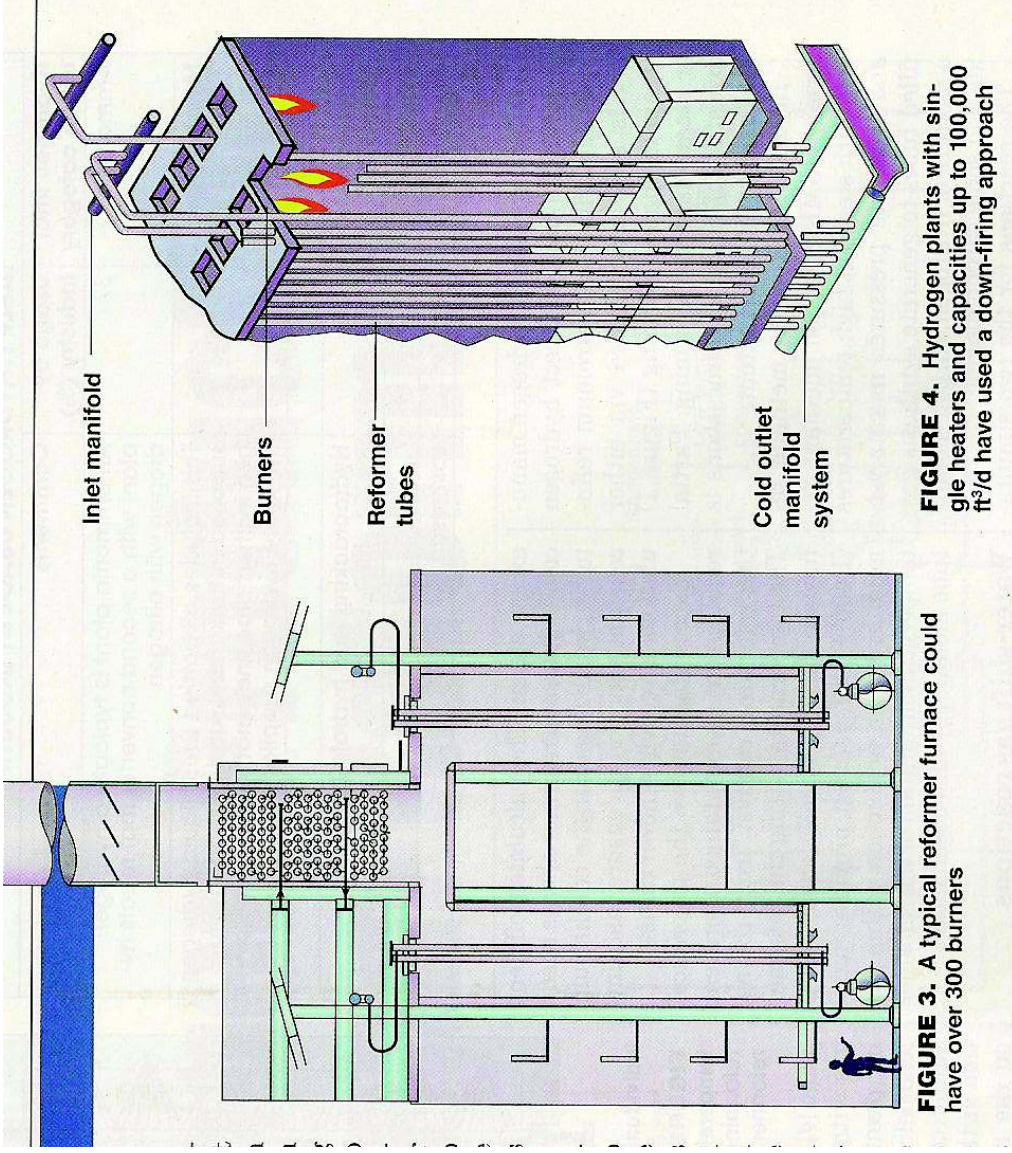
# estimation cost for Hydrogen

- **from DOE**  
100kg/day 8.09\$/kg - 1000kg/day 4.15\$/kg  
to reach 3.00\$/kg the electricity cost must be below than 4¢ to 5.5¢ per kWh  
**from Riso National Lab (Denmark)**  
**4.8 \$/Gj for H2 production assuming an electricity price of 3.6\$/Gj (equivalent to 29\$/barrel oil)** to 7.8 \$/Gj  
for CH4 production (**48\$/barrel oil**) or 71 cents /kg H2 using HHV at 950°C for SOECs  
if we take into account the degradation propertie of HHV it gives 108 cents/kg or **46\$/barrel**

**from ENSMP/CEA (2009) thesis R.Rivera-Tinoco**  
for a 1.5 kg/s hydrogen production and a cost of electricity between **40to 50 euros /MWh**  
**the cost is between 1.9 to 2.2 euros /kg H2**  
(electrolyser 900°C with high temperature water 523K from EPR)

**notice the price of crude oil barrel is between 72 to 112\$/barrel in 2010**



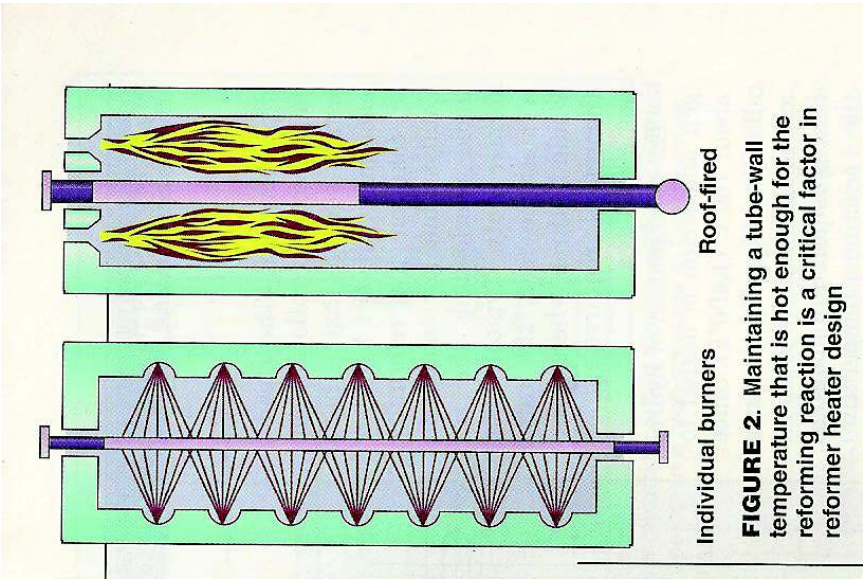


**FIGURE 4.** Hydrogen plants with single heaters and capacities up to 100,000 ft<sup>3</sup>/d have used a down-firing approach

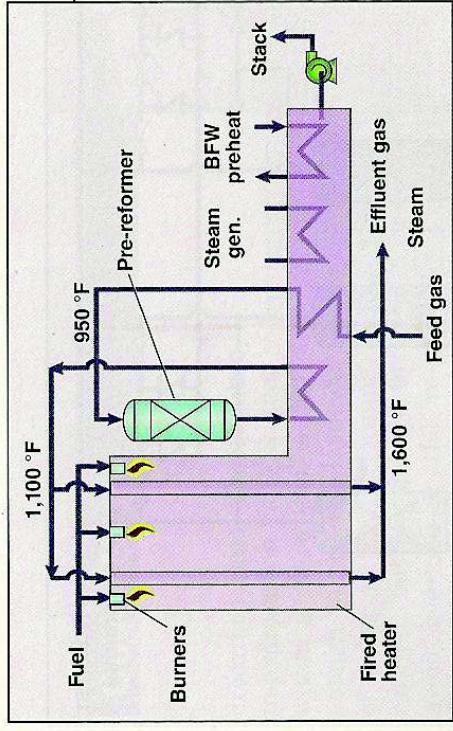
<b>TABLE 1. HYDROGEN USAGE BY INDUSTRY</b>		
<b>Hydrogen final usage category</b>	<b>Usage by industry (%)</b>	<b>Comments</b>
Ammonia	37	An ammonia plant is typically a hydrogen plant with a second converter that reacts hydrogen with nitrogen
Merchant	3	This includes all bottled users, liquid hydrogen supplied in tank trucks, and gaseous hydrogen in short pipe lines (not including the over-the-fence hydrogen suppliers)
Methanol	10	
Refinery hydro-generation	19	Hydrocracking and hydrotreating
Cryogenics	17	
Refinery fuel gas	14	Last resort

as well as from direct hydrogen manu- | excess steam. The calculated effluent |

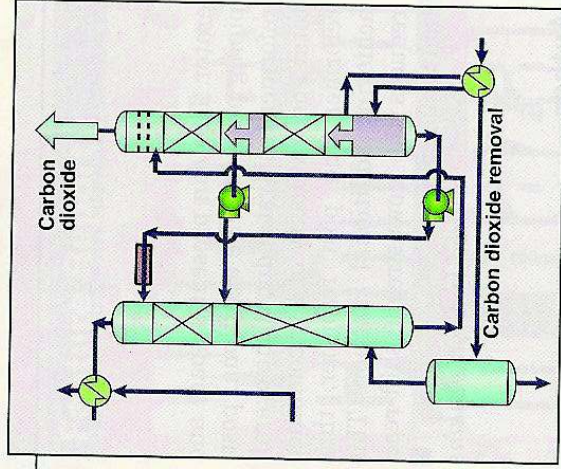




**Individual burners**      **Roof-fired**  
**FIGURE 2.** Maintaining a tube-wall temperature that is hot enough for the reforming reaction is a critical factor in reformer heater design

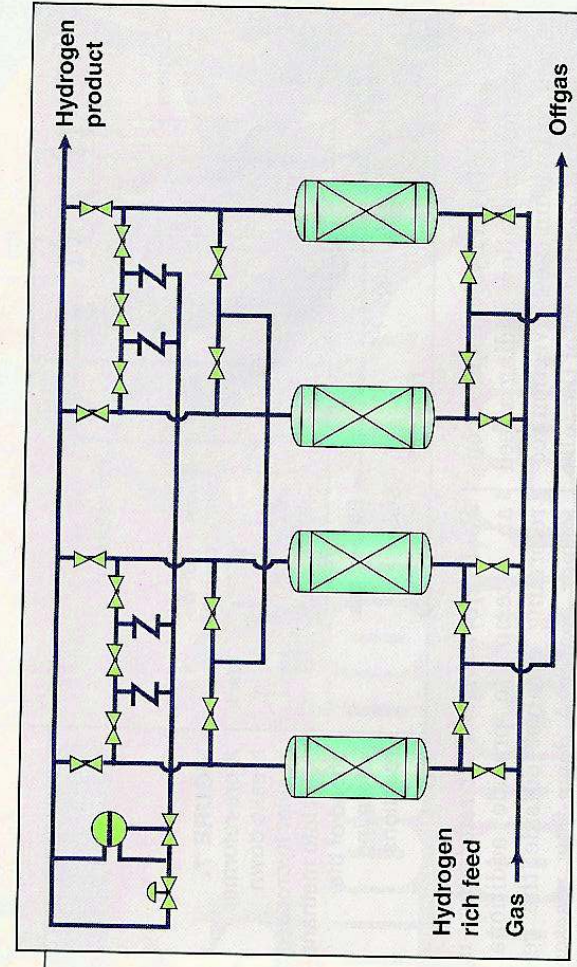


**FIGURE 7.**  
 A pre-reformer breaks down heavier hydrocarbons into methane ahead of the reforming reactions



**FIGURE 5.** Most older units remove carbon dioxide from the hydrogen-rich gas with a solvent

steam generator. BFW is fed through



**FIGURE 6.** A PSA unit separates carbon monoxide, carbon dioxide and unconverted hydrocarbons from hydrogen. Adsorbers operate in a high-pressure to low-pressure cycle to adsorb and then release contaminants

Hydrogen purification



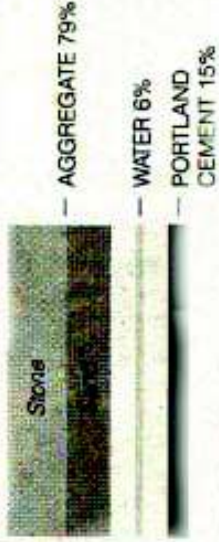


## New cements for CO<sub>2</sub> storage

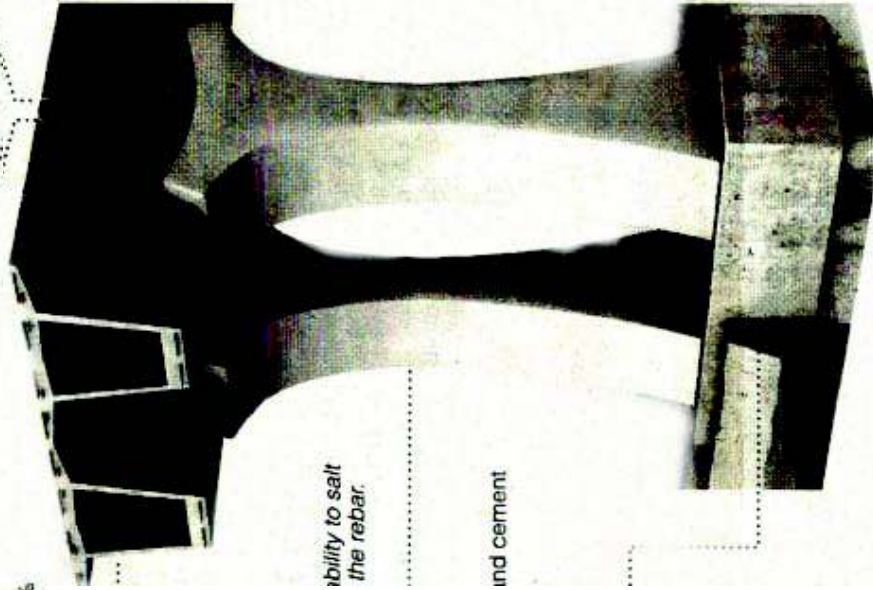
- new cements are able to Storage 0.6 ton
- of CO<sub>2</sub> per ton of cement
- It gives a positive material balance for CO<sub>2</sub>

# The Remix for a Planet Growing Warm

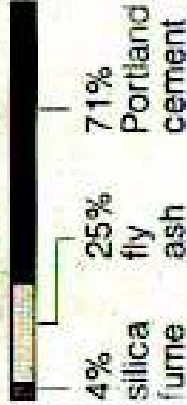
A Typical Concrete Mixture



CONCRETE  
STEEL BARS (REBAR)



## BOX GIRDER



■ 29 percent reduction in CO<sub>2</sub>

■ Silica fume reduces permeability to salt from road surface, protecting the rebar.

## PIERS

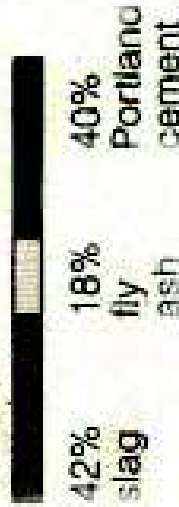


15% Portland cement

■ 85 percent reduction in CO<sub>2</sub>

■ Fly ash adds strength.

## FOOTINGS

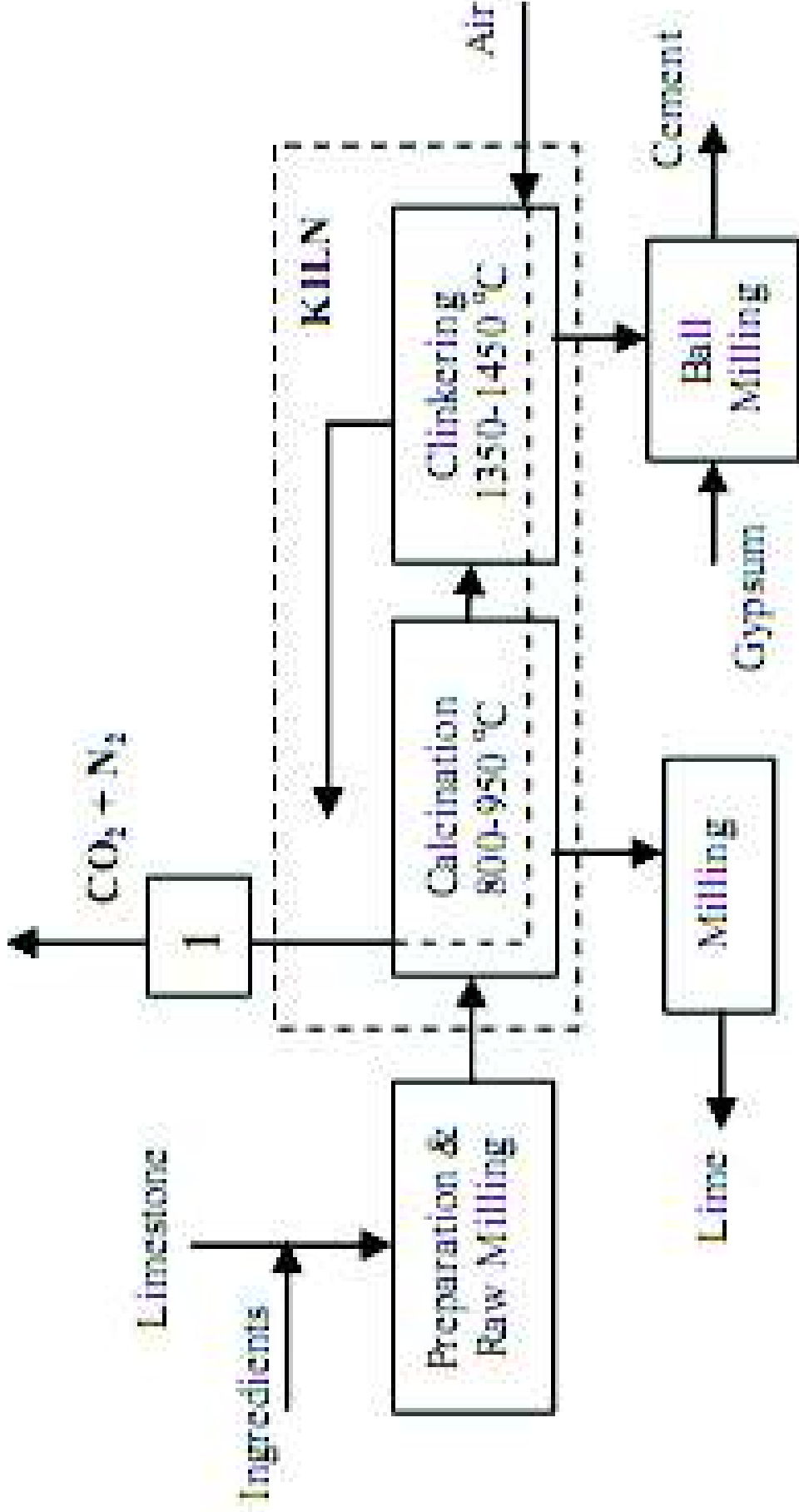


■ 60 percent reduction in CO<sub>2</sub>

■ Slag improves resistance to corrosive sulfates in the soil.

Sources: Kevin A. MacDonald, Cemstone Products Company;  
Richard D. Stehly, American Engineering Testing

# Lime and cement processing



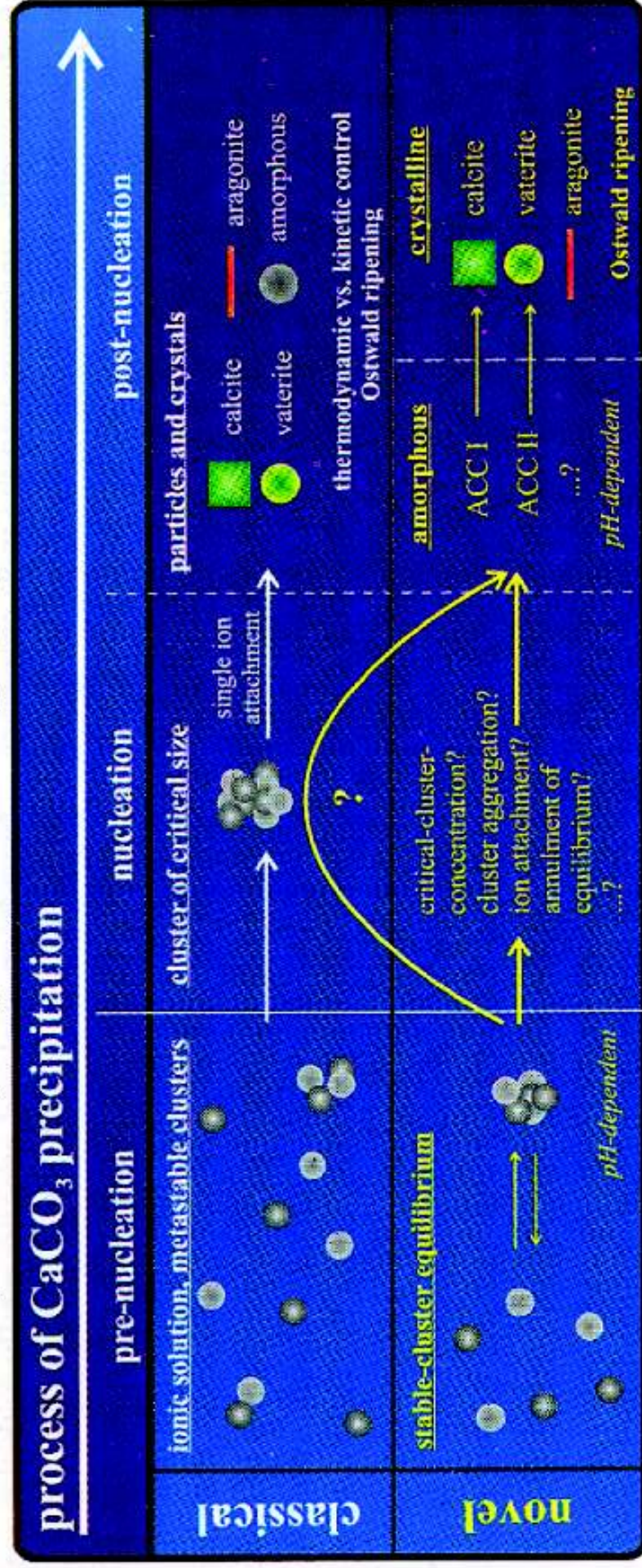
Flow sheet of a typical, state-of-the-art process for the manufacture of lime and cement. After a preparation and raw milling step, lime is produced through calcination within a kiln. Cement is produced in a further clinkering step and much more elevated temperatures. Most CO<sub>2</sub> is produced from the decomposition of carbonates and burning of kiln fuel. Final products are obtained following fine milling steps.



# Nucleation of calcium carbonate clusters

Denis Gebauer, Antje Völkel, Helmut Cölfen\*

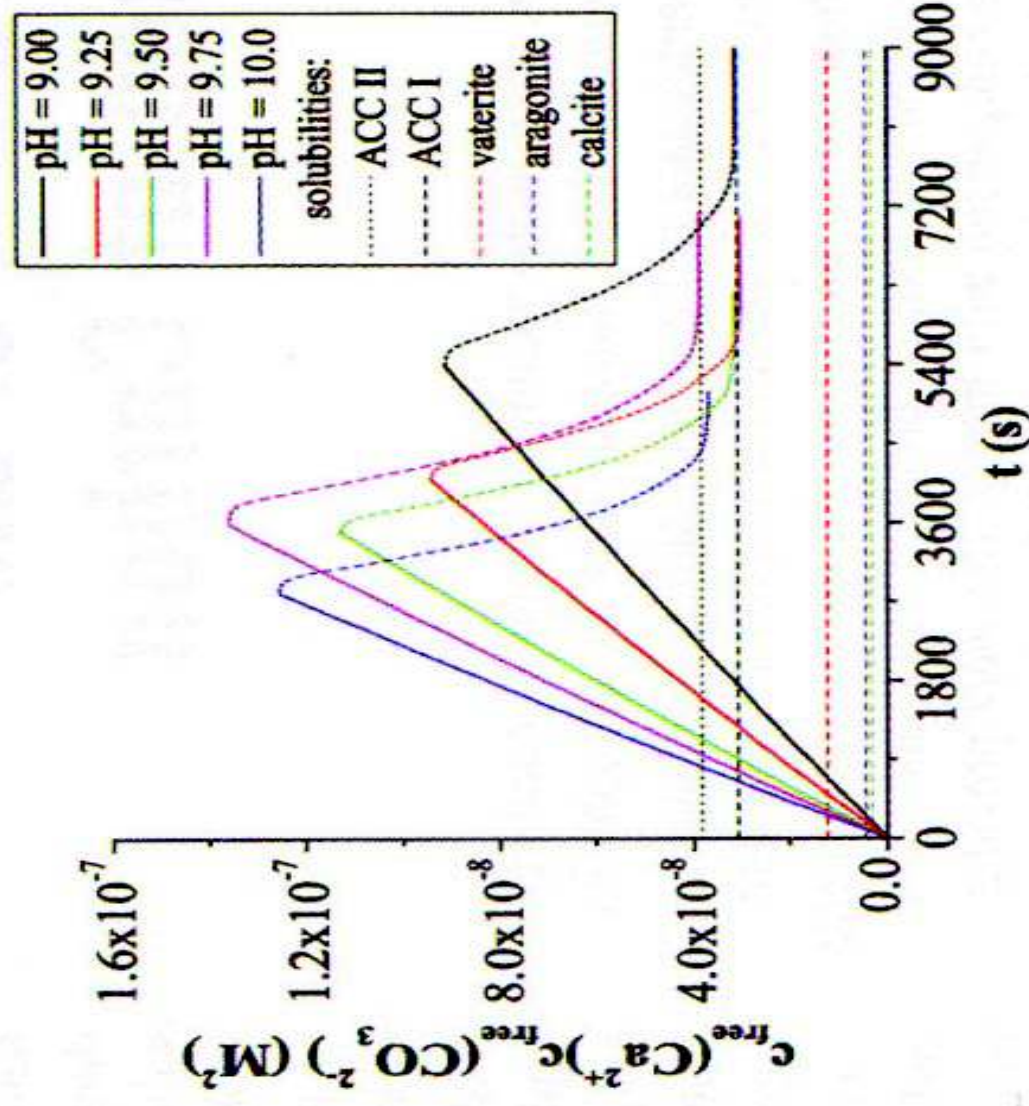
SCIENCE 322, 1819-1822 (2008), www.science mag.org /cgi/content/full/322/5909/1819/DC1

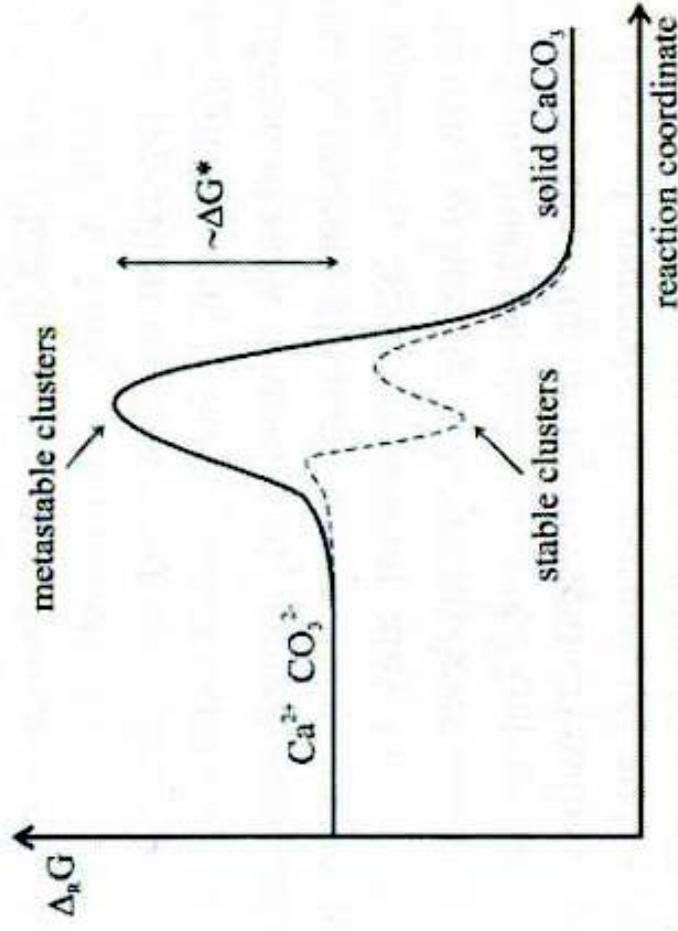


**Fig. 4.** Schema of the classical and novel view on precipitation (not to scale). Prenucleation-stage calcium carbonate clusters provide an early precursor species of different ACC phases giving rise to an alternative crystallization-reaction channel.



**Fig. 3.** Time development of the free ion product. Shown are averaged values obtained from a sample of three measurements. Because averaging is not appropriate during nucleation, the particular developments are indicated by dashed lines. We find two different ACC phases with solubility products of  $\sim 3.1 \times 10^{-8} \text{ M}^2$  (ACC I) and  $\sim 3.8 \times 10^{-8} \text{ M}^2$  (ACC II), corresponding to the pH dependency of the prenucleation cluster equilibrium. Also given are the solubilities of vaterite, aragonite, and calcite (27) (SOM section 2.5.)





**Fig. 2.** Schematic illustration of the free reaction enthalpy  $\Delta_r G$  versus the reaction coordinate. In the classical view (bold line), metastable clusters form and nucleation occurs when the critical nucleation enthalpy  $\Delta G^*$  is overcome. In fact, stable clusters (dashed line) are formed with an activation barrier negligible compared to thermal energy. The structure and depth of the indicated minimum remain unknown, as well as the height of the activation barrier for nucleation.

# Polymer synthesis from CO<sub>2</sub>

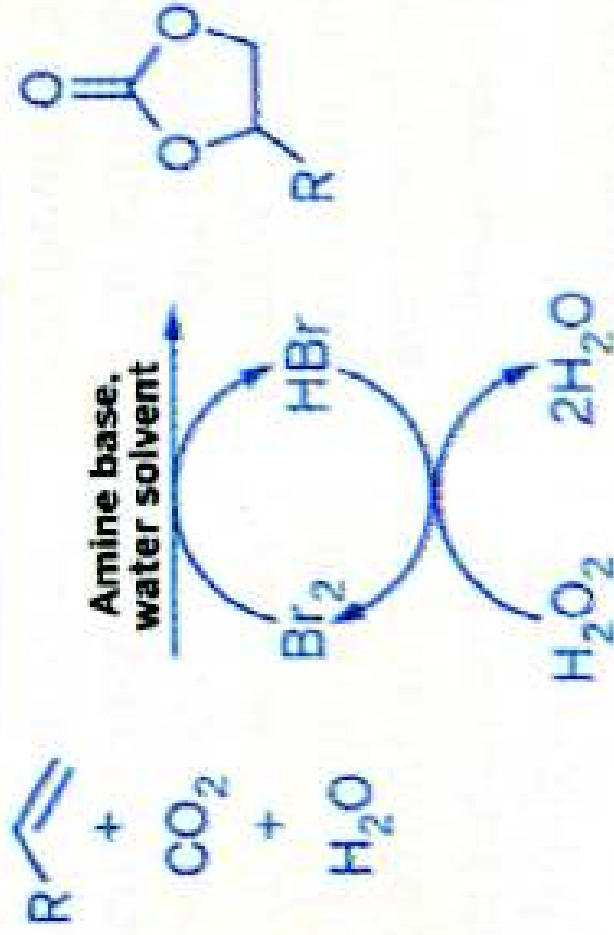
- One of the main fields for CO<sub>2</sub> polymerisation is to produce polycarbonate material which are biodegradable molecules and are able to store 50% of CO<sub>2</sub> in the weight
- It decreases the consumption of hydrocarbons of 50%



# WHAT CAN WE DO WITH CO<sub>2</sub>?

ACS MEETING NEWS: Scientists are trying to find ways to convert the plentiful greenhouse gas into fuels and other value-added products

BY JEFFREY M. H. SMITH



R = H, alkyl, phenyl

## GREENER CARBONATES

Eghbali and Li fashioned a direct route to cyclic carbonates from an olefin and CO<sub>2</sub> that bypasses the extra step of making an epoxide starting material.

Polymer synthesis with CO<sub>2</sub> give polycarbonates Which can storage 50% Of CO<sub>2</sub> in weight

### starting material.

C&EN Chemical Engineering News april 30,2007 ,p 11-17  
Green Chemistry 2007,9,213

Geoffrey W. Coates(Cornell University 1960)

\*\*\*\* catalyst to incorporate CO<sub>2</sub> into polymers

( B diminate Zinc acetate and salen cobalt carboxylate complexes)

Copolymerization of epoxide with CO<sub>2</sub>: biodegradable polycarbonates

\*\*\*\* Novomer Company (Ithaca NY)

Polymers which contain 30%- 50% CO<sub>2</sub> by weight

• J Am Chem Soc. 2007,129,4948 Coates groups aluminium-cobalt catalyst  
Double carbonylation of epoxides

• Chem. Commun 2007,657

Coates groups

epoxides, aziridines, lactones, oxazolines;  
ring expansion carbonylations



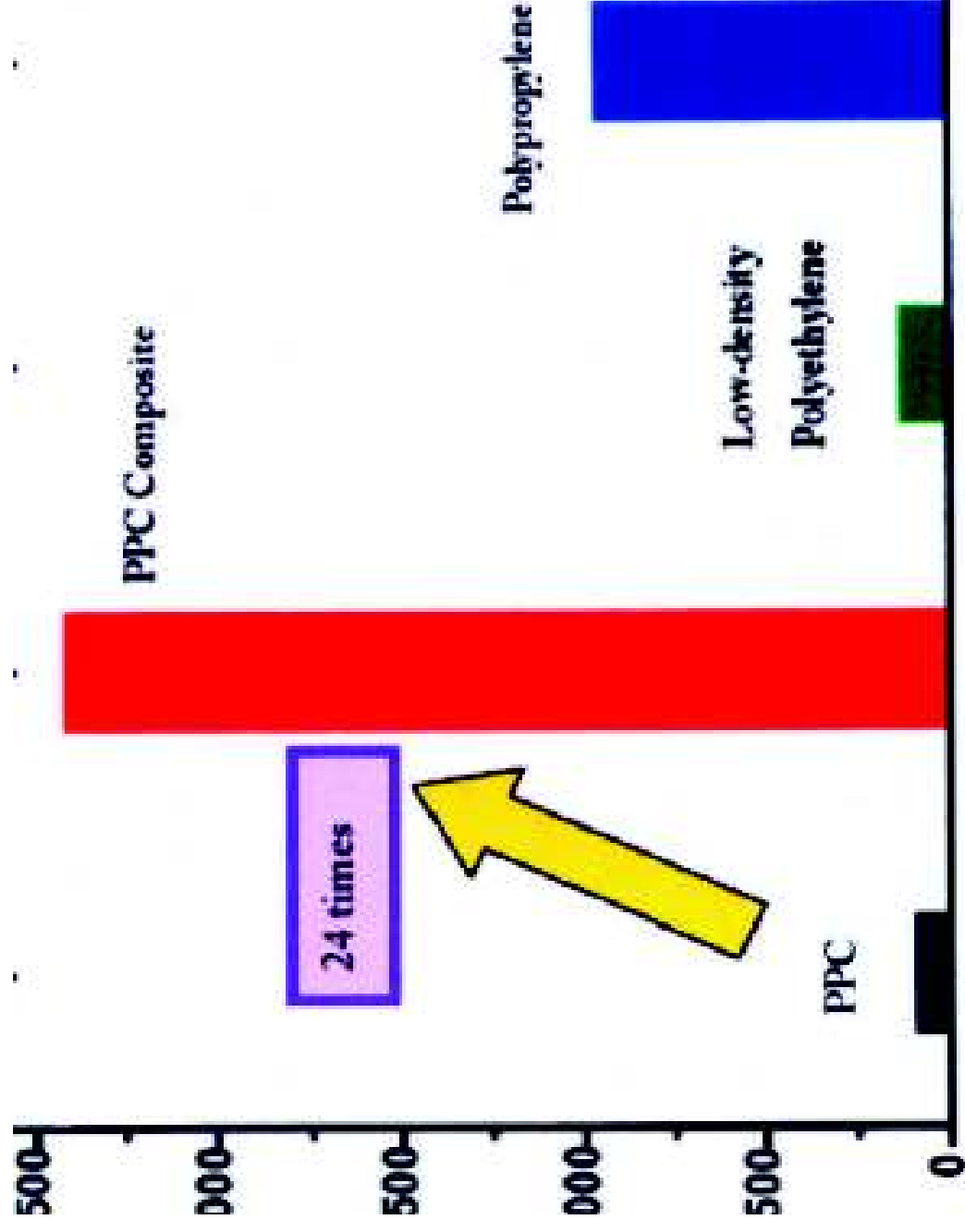


Figure Modulus data for PPC, PPC composite, and general-purpose plastics

Significant Property Improvement of plastic made from carbone dioxide

AIST Nov 18, 2008

Hiroshi Shimizu, Li Yongjin, Nanotechnology Reseach Institute ,Dir Nobutsugu Minami  
 Of National institute of Advanced Industrial Science and Technology (AIST)  
 President Hiroyuki Yoshikawa

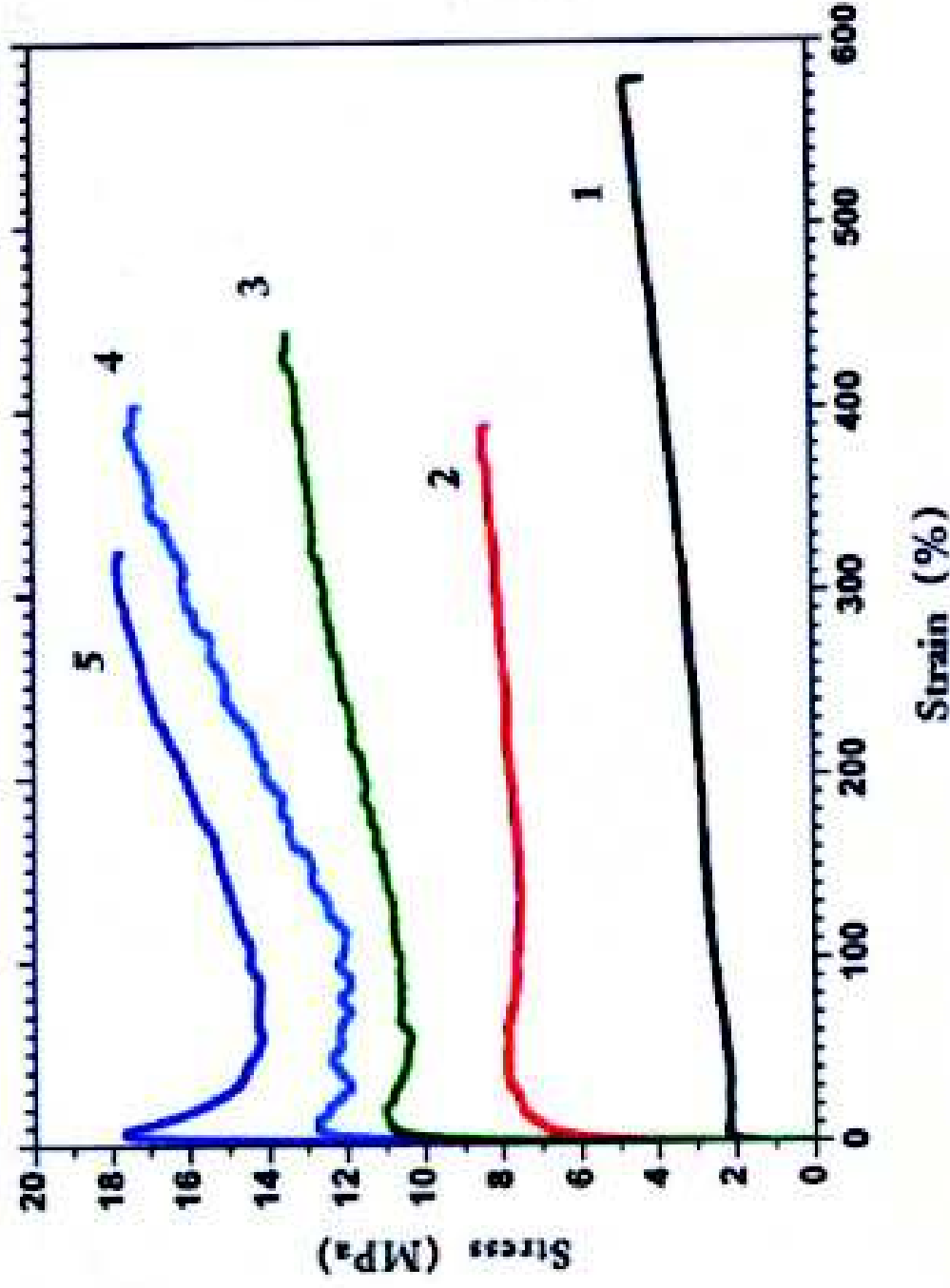


Figure 1 Stress – strain curves of PPC and PPC composites

[Curve 1: pure PPC, Curves 2 to 5 : PPC composites, (2 : PPC/X=70/30, 3 : PPC/X/Y=70/30/2.5, 4 : PPC/X/Y=70/30/10, 5 : PPC/X/Y=70/30/5)]

Significant Property Improvement of plastic made from carbone dioxide  
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 President Hiroyuki Yoshikawa

Table 1 Mechanical properties at room temperature (25°C)

Sample	Modulus(MPa)	Strength(MPa)	Elongation at break(%)	Tg (°C)
PPC	101	4.8	578	30.4
PPC/X=70/30	1564	8.4	390.6	36.7
PPC/XY=70/30/5	2431	17.9	322	39.8
Low-density polyethylene	142	16.6	616	-128
iso-polypropylene	979	26.1	1077	-0.1

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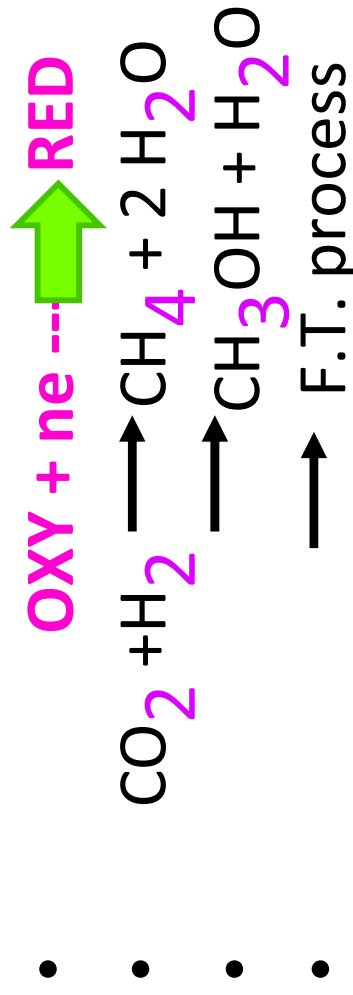


# CO2 for ENERGY STORAGE

- energy storage from decarbonated sources
  - \*\*\*  
*technical and financial data*
  - \*\*\*  
*capture unit from exhaust gas*
  - \*\*\*  
*thermodynamic data*
  - \*\*\*  
*Redox processes and catalysist material*

# CO<sub>2</sub> a good candidat for ELECTRICAL ENERGY STORAGE

Great advantages of chemical plant with  
REDOX reactions for carbon recovery:large  
chemical facilities



• The key step is hydrogen production

# energy management and electrical storage

- evolution of the fossil carbon fields (including coal, petroleum, gas)



◦ electrical energy storage

◦ carbon recovery

◦ energy cost and energy storage cost

◦ geopolitical problems of the energy resources

# European set plan 2008

a reversible storage of CO2  
capture

***gives carbon resources  
for the futur of our civilization***

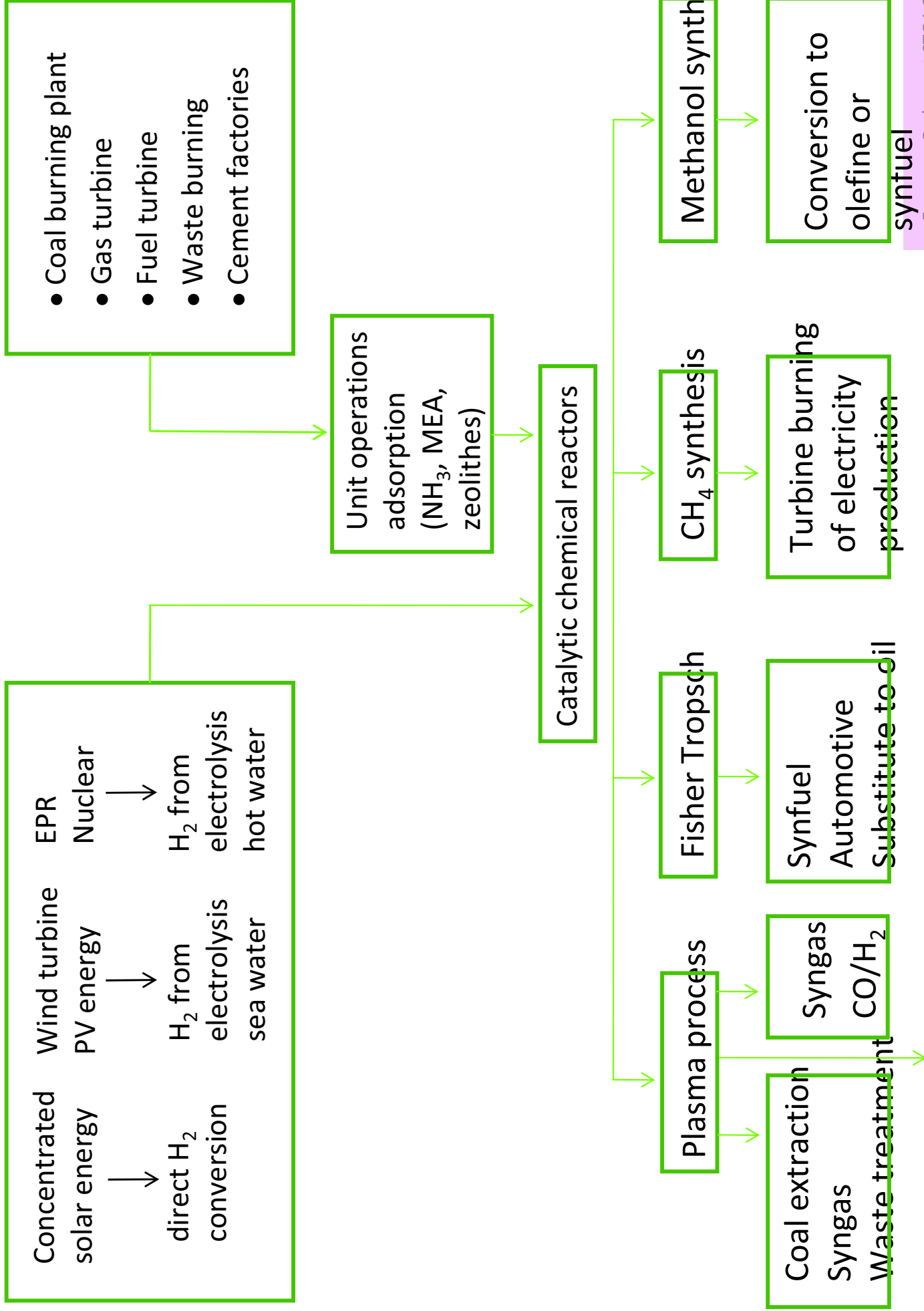


## Financial aspects

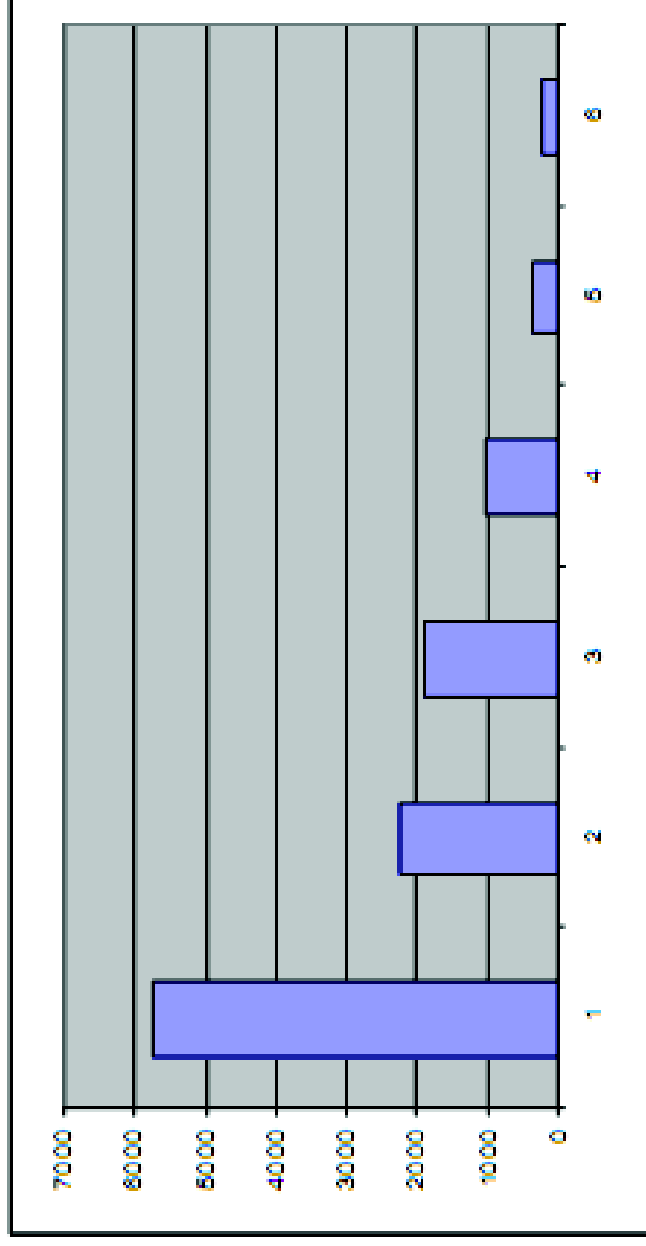
one of the main working parameters is  
how much  
it was the deal of Kyoto program for  
carbon dioxide regulation  
it is the challenger of

Cancun conference

this week (30 nov-7 dec 2010)



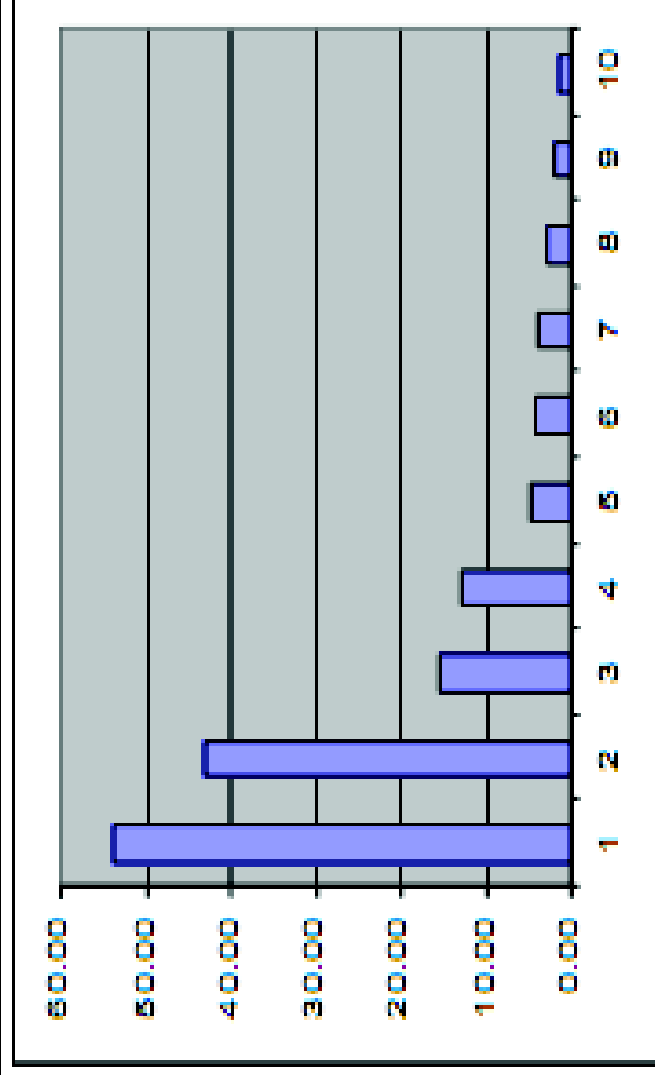
# Total emissions USA 2002 in MMt (10<sup>6</sup>t)



1. Total US	5752	%
2. Electric Power	2250	39
3. Transportation	1868	32
4. Industrial Processes	1042	18
5. Residential Homes	365	6
6. Commercial Buildings	227	4

U.S. 2002 CO<sub>2</sub> emissions in MMt: Total, Electric Power, Transportation, Industrial, Residential and Commercial

## Total emissions USA 2002 in MMT (10<sup>6</sup>t) (non-energy related processes)



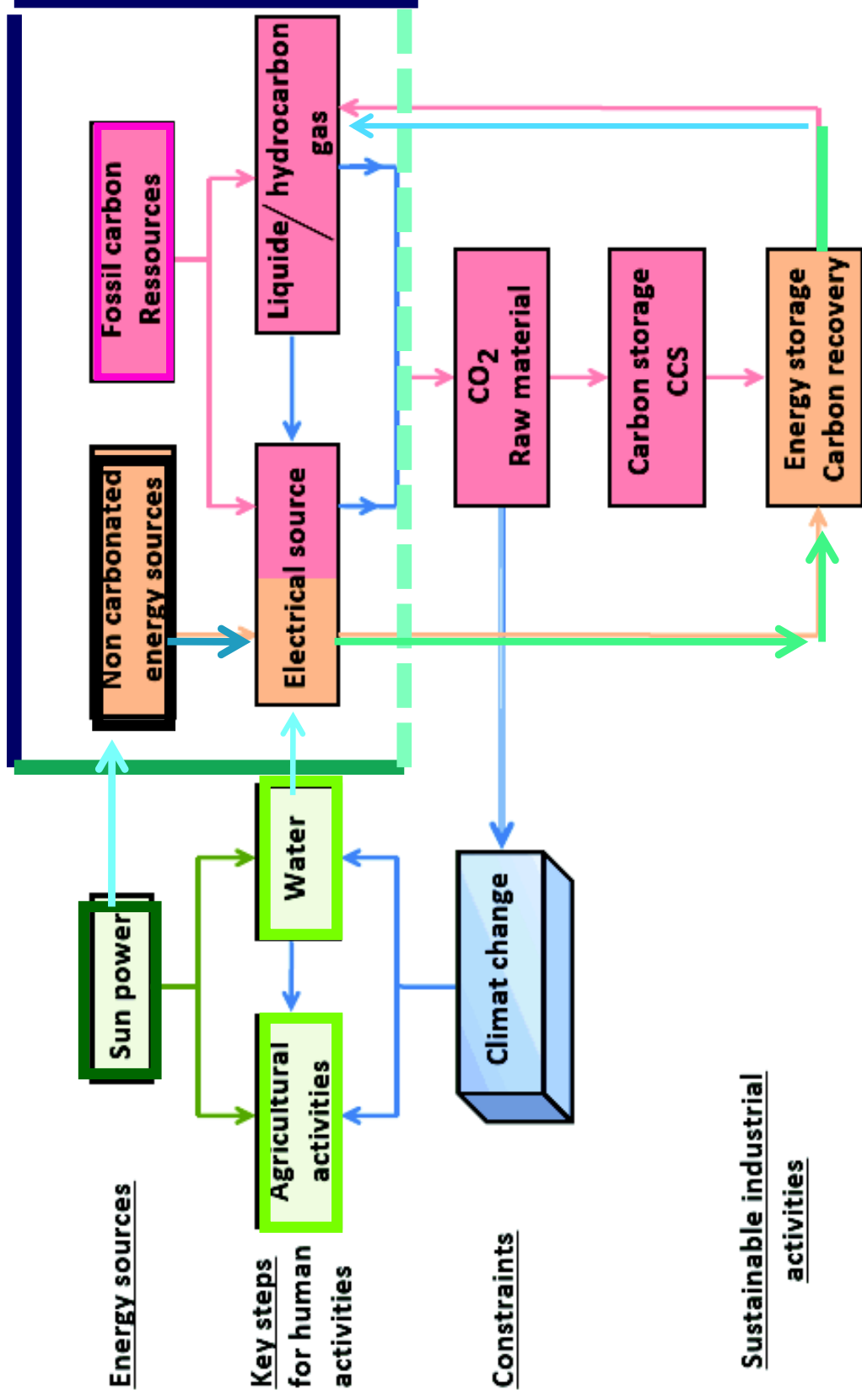
3. U.S. Industry 2002 CO<sub>2</sub> emissions in MMT: non-energy related processes



# energy efficiency of coal energy processes

- coal burning system for electrical power station
- in the main countries 30%
- new plants 37%
- supercritical news plants 45 to 58%

# energy from industrial processes



# control of carbon dioxide level

# Fourth Part

- main ways for energy storage from electron to carbon recovery by using CO<sub>2</sub> molecule
- Electron to chemical synthesis :Hydrogen + CO<sub>2</sub>
  - to Methanol
  - to Methane
  - to synfuel by FT processes
- electron to plasma processes
  - thermal or non equilibrium plasmas
- Photon to thermolysis of water or CO<sub>2</sub> dissociation